

```

C *****
C
C          PEDROP
C THIS PROGRAM COMPUTES PRESSURE DROP VERSUS MASS FLOW RATE
C OF A UNIFORMLY HEATED SUBCHANNEL MADE UP OF FOUR RODS
C ARRANGED IN A SQUARE ARRAY. THE COOLANT AT THE INLET IS SINGLE
C PHASE PRESSURIZED WATER. THERMODYNAMIC PROPERTIES ARE VALID FOR THE
C PRESSURE RANGE OF 5.514 TO 11.029 MPA (800 TO 1600 PSIA).
C
C *****
C
C NOMENCLATURE AND UNITS OF INPUTS.
C P      PRESSURE(MPA)
C DROD   ROD DIAMETER(M)
C PITCH  ROD CENTER-TO-CENTER DISTANCE(M)
C TL     CHANNEL AXIAL LENGTH(M)
C TIN    COOLANT INLET TEMPERATURE(K)
C TSAT   SATURATION TEMPERATURE(K)
C HIN    INLET ENTHALPY (KJ/KG)
C NQ     NUMBER OF HEAT FLUXES
C Q      HEAT FLUX(MW/M**2)
C MASS   HIGHEST MASS FLOW RATE(KG/SEC)
C DEC    MASS FLOW RATE DECREMENTS(KG/SEC)
C MINM   LOWEST MASS FLOW RATE(KG/SEC)
C LBOT   BOTTOM UNHEATED LENGTH (M)
C LTOP   TOP UNHEATED LENGTH (M)
C LEBOT  BOTTOM, EQUILEVENT LENGTH TO ACCOUNT FOR FORM LOSS(M)
C LETOP  TOP
C IFLAG  IFLAG>0 => NO CALCULATION OF ACCELERATION PR. DROP
C JFLAG  JFLAG>0 => USE DEVIDED FACTOR IN PRESSURE RANGE
C        14.7 PSI < P < 100 PSI
C KFLAG  KFLAG>0 => TWO PHASE MULTIPLIER IN SUBCOOLED BOILING REGION =1
C
C ZSC    AXIAL POINT OF INCEPTION OF SUBCOOLED BOILING(M)
C ZB     AXIAL POINT OF INCEPTION OF BULK BOILING(M)
C ZV     AXIAL POINT OF INCEPTION OF SINGLE PHASE VAPOR(M)
C
C COMMON Q(30)
C CHARACTER*64 FINPUT,FOUTPUT
C REAL MASS,MDOT,MINM,LEBOT,LTOP,LEBOT,LETOP
C DATA C4,C5,C6,C7,C8/958.75,-0.8566,2619410.618,-4.995E10,3.403E5/
C DATA C9,C10,C11,C12/1.0665545,1.02E-8,-2.548E-15,2589600./
C DATA C13,C14,C15,C16/6.350E-3,-1.0582E-9,1.0764,3.625E-10/
C DATA C17,C20,C23,C24,C26/-9.063E-17,461.7,647.3,1.3,0.3/
C DATA PI/3.1415926/
C CALL LINK('UNIT5=IPEDROP,UNIT6=(OPEDROP,CREATE,TEXT),UNIT59=TTY//')
C 1)
C WRITE(*,888)
C READ(*,887)FINPUT
C WRITE(*,886)
C READ(*,887)FOUTPUT
C OPEN(5, FILE=FINPUT)
C OPEN(6, FILE=FOUTPUT,STATUS='NEW')
888 FORMAT(' INPUT DATA FILE NAME'\)
887 FORMAT(A)
886 FORMAT(' OUTPUT DATA FILE NAME'\)
C CALL ERRSET(208,256,-1,0,0,0)
C READ(5,1001) NSET
C DO 700 K=1,NSET
C   LBOT=0.0
C   LTOP=0.0
C   IFLAG=0
C   JFLAG=0
C   KFLAG=0
C   LEBOT=0.
C   LETOP=0.
C   DETOP=0.
C   DFTOP=0.
C   DEBOT=0.
C   DFBOT=0.
C   WRITE(6,1) K
1 FORMAT(///3X,'RESULTS OF DATA SET NUMBER = ',I5//)
C READ(5,1000) P,DROD,PITCH,TL,TIN,TSAT,HIN
C READ(5,1000) MASS,DEC,MINM,LEBOT,LTOP,LEBOT,LETOP
C READ(5,1001) NQ,IFLAG,JFLAG,KFLAG
C READ(5,1000) (Q(I),I=1,NQ)
C A11 = 2.*C26/(C24+C20)
C A13 = A11*(1.+C26)
C A12 = 1./A13
C A15 = 1./C23

```

```

C
C CALCULATION OF HYDRAULIC DIAMETER.
C
  A = PITCH**2-PI*DROD**2/4.
  PW = PI*DROD
  D = 4.*A/PW
  WRITE(6,3)
3  FORMAT(3X,'GEOMETRICAL PARAMETERS AND INLET CONDITIONS')
  WRITE(6,4)
4  FORMAT(3X,'*****')
  WRITE(6,5) A,PW,D,TL
5  FORMAT(3X,'CHANNEL FLOW AREA = ',E13.6,1X,'M**2'/3X,'WETTED PERIME
  1TER = ',E13.6,1X,'M'/3X,'HYDRAULIC DIAMETER = ',E13.6,1X,'M'/3X,'C
  2HANNEL AXIAL LENGTH = ',E13.6,1X,'M')
  WRITE(6,6) P,TIN
6  FORMAT(3X,'INLET PRESSURE = ',F10.4,1X,'MPA'/3X,'INLET TEMPERATURE
  1 = ',F10.4,1X,'K')
  DO 700 I=1,NQ
  WRITE(6,7)
7  FORMAT(/3X,'*****')
  WRITE(6,10) Q(I)
10  FORMAT(3X,'HEAT FLUX = ',E13.6,1X,'MW/M**2')
  WRITE(6,20)
20  FORMAT(3X,'*****')
  MDOT = MASS
  IF(Q(I).EQ.0.0) MMP = 31
  IF(Q(I).GT.0.0) MMP = 30
C
C DO 700 J=1,MMP
C
23  DFNONB = 0.0
  DENONB = 0.0
  DANONB = 0.0
  HFO = 0.0
  DTNONB = 0.0
  DTSUB = 0.0
  DEBB = 0.0
  DFBB = 0.0
  DABB = 0.0
  DESUB = 0.0
  DASUB = 0.0
  DFSUB = 0.0
  DTSUB=0.0
  DTBB = 0.0
  DEVAP = 0.0
  DAVAP = 0.0
  DFVAP = 0.0
  DTVAP = 0.0
  DROP = 0.0

C
C FLUID PROPERTIES AT INLET.
C
  TBA = TIN
  CPF = CP(TBA)
  TKW = TKCOOL(TBA,P)
  UBF = UF(TBA)
C
  RHOFI = RHOF(TBA)
  PP=P*1.E6
  CALL STATE(PP,TBA,TBA,ROV,RHOFI,EV,EL,TTSAT,HVS,HLS,DTSTP,
1  DELDP,DEVDP,DELDI,DEVDT,DRLDP,DRVDP,DRLDI,DRVDT,IOP,IERR)
  IF(MDOT.LT. MINM) GO TO 700
  IF(MDOT .LE. 0.) GO TO 700
  VELI = MDOT/(RHOFI*A)
  G = VELI*RHOFI
  WRITE(6,40) MDOT,G
40  FORMAT(/3X,'MASS FLOW RATE = ',E13.6,1X,'KG/SEC'/3X,'MASS FLUX = '
  1,E13.6,1X,'KG/SEC-M**2')

C
C CALCULATION OF THE POINT OF BUBBLE DETACHMENT (ASSUMED = ZSC) USING
C THE SAHA AND ZUBER METHOD.
C
  IF(Q(I).EQ.0.0) GO TO 53
  PEC = G*D*CPF/TKW
  IF(PEC.LE.70000.) DELSUB = .0022*Q(I)*1.E6*D/TKW
  IF(PEC.GT.70000.) DELSUB = 153.8*Q(I)*1.E6/(G*CPF)
  TFZSC = TSAT-DELSUB
  ZSC = D*G*CPF*(TFZSC-TIN)/(4.*Q(I)*1.E6)
  WRITE(6,50) PEC,DELSUB,TFZSC,ZSC
50  FORMAT(3X,'PECLET NUMBER = ',E13.6/3X,'DELTA-T SUB = ',E13.6,1X,'K
  1'/3X,'FLUID TEMP. AT ZSC = ',E13.6,1X,'K'/3X,'ZSC = ',E13.6,1X,'M'
  2)

```

```

53 IF(ZSC.GT.TL.OR.Q(I).EQ.0.0) ZSC = TL
   IF(ZSC.LT.0.0) ZSC=0.0
C
C NON-BOILING PRESSURE DROPS.
C   WRITE(6,121) VELI
C
   IF(VELI.GT.0.0) RE = G*D/UBF
   IF(VELI.GT.0.0) FRIC = .316/RE**.25
   IF(VELI.LE.0.0) GO TO 55
   HFO = .023*TKW/D*(G*D/UBF)**.8*(UBF*CPF/TKW)**.4
   TBA = TIN+0.5*(TFZSC-TIN)
C   RHOFB = RHOF(TBA)
   PP=P*1.E6
   CALL STATE (PP,TBA,TBA,ROV,RHOFB,EV,EL,TTSAT,HVS,HLS,DTSDP,
1 DELDP,DEVDP,DELDLT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IOP,IERR)
55 IF(Q(I).EQ.0.0) RHOFB=RHOFI
   IF(VELI.GT.0.0) DFNONB = ZSC*FRIC*G**2/(2.*D*RHOFB)
   DENONB = RHOFB*9.81*ZSC
   DFBOT=(LBOT+LEBOT)*FRIC*G**2/(2.*D*RHOFI)
   DEBOT=RHOFI*9.81*LBOT
   DTBOT=DEBOT+DFBOT
   TBA = TFZSC
   RHOZSC = RHOF(TBA)
   PP=P*1.E6
   CALL STATE (PP,TBA,TBA,ROV,RHOZSC,EV,EL,TTSAT,HVS,HLS,DTSDP,
1 DELDP,DEVDP,DELDLT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IQP,IERR)
   IF(Q(I).EQ.0.0) RHOZSC=RHOFI
   IF(VELI.LE.0.0) GO TO 59
   IF(ZSC.GT.0.0) DANONB=G**2*(1./RHOZSC-1./RHOFI)
   IF(IFLAG.GT. 0) DANONB=0.0
   IF(ZSC.LT. TL) GO TO 59
   DFTOP=(LTOP+LETOP)*FRIC*G**2/(2.*D*RHOFB)
   DETOP=RHOFB*9.81*LTOP
   DTTOP=DETOP+DFTOP
59 DTNONB = DFNONB+DENONB+DANONB
C   WRITE(6,60) RE,FRIC,RHOFB,RHOZSC,HFO
60 FORMAT(3X,'REYNOLDS NUMBER = ',E13.6/3X,'FRICTION FACTOR = ',E13.6
1/3X,'AV. NON-BOILING BULK FLUID DENSITY = ',F10.3,1X,'KG/M**3'/3X,
2'FLUID DENSITY AT ZSC = ',F10.3,1X,'KG/M**3'/3X,'COEFFICIENT OF HE
3AT TRANSFER = ',F10.3,1X,'W/M**2-K')
   IF(ZSC.GE.TL.OR.Q(I).EQ.0.0) GO TO 625
C
C DETERMINATION OF ZB.
C
   TBA = TSAT
   RHOFZB = RHOF(TBA)
   PP=P*1.E6
   PB=P-0.004*P
100 PPB=PB*1.E6
   CALL STATE (PPB,TBA,TBA,ROV,RHOFZB,EV,EL,TTSAT,HVS,HLS,DTSDP,
1 DELDP,DEVDP,DELDLT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IQP,IERR)
   CALL STATE (PPB,TTSAT,TTSAT,RHOGZB,RHOFZB,EV,EL,TTTSAT,HVS,HLS,DTSD
1P,DELDLP,DEVDP,DELDLT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IQP,IERR)
   HF=HLS/1.E3
   UBF=UF(TSAT)
   UBG=UG(TSAT)
C   WRITE(6,121) RHOGZB,RHOFZB,HLS
C   RHOGZB = RHOG(TBA,PB)
   TBA=.5*(TSAT+TFZSC)
   RHOSUB=.5*(RHOFZB+RHOZSC)
   CPF = CP(TBA)
   ZB = MDOT*(HF-HIN)/(PI*Q(I)*1.E3*DROD)
   IF(ZB.GT.TL) ZB=TL
   IF(ZB.LT.0.0) ZB=0.0
   IF(ZB.LT. ZSC) ZSC=ZB
C
C SUBCOOLED BOILING PRESSURE DROPS.
C
   DESUB = RHOSUB*9.81*(ZB-ZSC)
   IF(ZB.GT.0.0) DASUB=(G**2*(1./RHOFZB-1./RHOZSC))
   RE=G*D/UF(TBA)
   IF(VELI.GT.0.0) FRIC=.316/RE**.25
C
C BRITISH UNITS USED FOR SUBCOOLED FRICTION PR. DROP CALCULATIONS.
C
   FPD = (G*737.73)**2*FRIC/(2.*32.2*3600.**2*D*3.281*RHOSUB*0.06243)
   TLBSTR= ((TSAT-273.15)*1.8+32.+60.*((Q(I)*.3169E6/.1E7)**.25/EXP(
1PB*.145E3/900.))- .766*Q(I)*.3169E6/(HFO*.1761))-32.)*5./9.+273.15
   PHLOMN = (1.2*((RHOFZB/RHOGZB)-1.)*.042**.824)

```

```

C      WRITE(6,120)
120  FORMAT(1X,'FPD,TLBSTR,PHLOMN,FACTOR,CORFAC')
C      WRITE(6,121) FPD,TLBSTR,PHLOMN,FACTOR,CORFAC
121  FORMAT(1X,8E13.6)
150  IF(G*737.73.LT.7.E5) CORFAC = 1.36+.0005*PB*.145E3+.1*(G*737.73/1.
1E6)-.000714*PB*.145E3*(G*737.73/1.E6)
      IF(G*737.73.GT.7.E5) CORFAC = 1.26-.0004*PB*.145E3+.119*(1.E6/(G*7
137.73))+.00028*PB*.145E3*(1.E6/(G*737.73))
      FSAT = PHLOMN*CORFAC+1.
      DEVID=(7.04-3.8*.042)*(1.172-1.7*PB)+3.4*PB-0.344
      IF(JFLAG .GT. 0) FSAT=FSAT/DEVID
      FOFISO = 1.+(TBA-TLBSTR)*(FSAT-1.)/(TSAT-TLBSTR)
      IF (TBA .LT. TLBSTR) FOFISO = 1.-0.001*Q(I)/HFO
      IF (KFLAG .GT. 0) FOFISO=1
      DFSUB = 47.867*FPD*(ZB-ZSC)*3.281*FOFISO
      IF(ZB .LT. TL) GO TO 160
      TEXIT=TIN+TL*PI*Q(I)*1.E6*DROD/(MDOT*CPF)
      PPB=PB*1.E6
      CALL STATE(PPB,TEXIT,TEXIT,ROV,RHOFTL,EV,EL,TTSAT,HVS,HLS,DTSDP,
1  DELDP,DEVDP,DELDT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IQP,IERR)
C      WRITE(6,121) RHOFTL
C      WRITE(6,121) TEXIT,RHOFTL
      DASUB=G**2*(1./RHOFTL-1./RHOZSC)
      DESUB=.5*(RHOFTL+RHOZSC)*9.81*(TL-ZSC)
      CPEXIT=CP(TEXIT)
      TKEXIT=TKCOOL(TEXIT,PB)
      UBFEX=UF(TEXIT)
      RE=G*D/UBFEX
      FRIC=.316/RE**.25
      DFTOP=(LTOP+LETOP)*FRIC*G**2/(D*RHOFTL*2.)
      DETOP=RHOFTL*9.81*LTOP
160  IF(IFLAG .GT. 0) DASUB=0.0

      DTTOP=DFTOP+DETOP
      DTSUB = DESUB+DASUB+DFSUB
C      WRITE(6,170)
C 170  FORMAT(1X,'CORFAC,FSAT,FOFISO,TBA,TLBSTR')
C      WRITE(6,121)CORFAC,FSAT,FOFISO,TBA,TLBSTR
C
C      ITERATIONS OF PRESSURE AT ZB.
C
      PBB = (P*1.E6-(DTNONB+DTSUB+DTBOT))
C      WRITE(6,121) PB,PBB
      PBITE = ABS((PBB/1.E6-PB)/PB)
      IF(PBITE.GT.0.00005) PB=PBB/1.E6
      IF(PBITE.GT.0.00005) GO TO 100
      IF (KFLAG .LE. 0) GO TO 162
      DANONB=DANONB+DASUB
      TBA=(TIN+TSAT)/2.

      IF(ZB .GE. TL) TBA=(TEXIT+TIN)/2.
      PPB=PB*1.E6
      CALL STATE(PPB,TBA,TBA,ROV,RHOFA,EV,EL,TTSAT,HVS,HLS,DTSDP,
1  DELDP,DEVDP,DELDT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IQP,IERR)
      DENONB=RHOFA*9.81*ZB
      DFNONB=DFNONB*(RHOFA/RHOFA)*(ZB/ZSC)
      DTNONB=DANONB+DENONB+DFNONB
      DESUB=0.0
      DASUB=0.0
      DFSUB=0.0
      DTSUB=0.0
162  WRITE(6,200) ZB
200  FORMAT(3X,'ZB = ',F10.4,1X,'M')

      IF(ZB.GE.TL) GO TO 625
C
C      DETERMINATION OF ZV.
C
      PV = (P-0.006*P)
C 300  HG = ENTHAG(PV)
300  PPV=PV*1.0E6
      CALL STATE(PPV,TSAT,TSAT,ROV,ROL,EV,EL,TTSAT,HVS,HLS,DTSTP,
1  DELDP,DEVDP,DELDT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IOP,IERR)
      HG=HVS/1.E3
      ZV = MDOT*(HG-HIN)/(PI*Q(I)*1.E3*DROD)
      IF(ZV.GT.TL) ZV=TL
      IF(ZV.LT.0.0) ZV=0.0
C
C      CALCULATION OF MARTINELLI-NELSON VOID FRACTION.

```

```

C
XZSC = -CPF*DELSUB/((HG-HF)*1.E3)
XZB = -XZSC/2.71828
XTTZB = (UBF/UBG)**.1*((1.-XZB)/XZB)**.9)*(RHOGZB/RHOFZB)**.5
RGZB = 1.-XTTZB/((XTTZB**2+20.*XTTZB+1.)**.5)

C
C DETERMINATION OF X(Z=TL)=XOUT
C
C HGPB=ENTHAG(PB)
PPB=PB*1.E6
CALL STATE (PPB,TSAT,TSAT,ROV,ROL,EV,EL,TTSAT,HVS,HL,S,DTSDP,
1 DELDP,DEVDP,DELDT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IQP,IEERR)
HGPB=HVS/1.E3
C WRITE(6,121) HVS
HOUT=TL*(PI*Q(I)*1.E3*DROD)/MDOT+HIN
XEOUT=(HOUT-HF)/(HGPB-HF)
XOUT=XEOUT-XZSC*EXP(XEOUT/XZSC-1.)
IF(XEOUT.GT. 1.0) XEOUT = 1.0
IF(XOUT.GT. 1.0) XOUT =1.0

C
C BULK BOILING PRESSURE DROPS.
C
XZV = 1.-XZSC*EXP(1./XZSC-1.)
IF(ZV.GE. TL) XZV=XOUT
IF(XZV.GT.1.0) XZV=1.0
XTTZV = (UBF/UBG)**.1*((1.-XZV)/XZV)**.9)*(RHOGZB/RHOFZB)**.5
RGZV = 1.-XTTZV/((XTTZV**2+20.*XTTZV+1.)**.5)
RHOB = RHOFZB-0.5*(RGZB+RGZV)*(RHOFZB-RHOGZB)
DEBB = RHOB*9.81*(ZV-ZB)
RHOZV=RHOFZB-RGZV*(RHOFZB-RHOGZB)
DZV = XZV**2/(RHOGZB*RGZV)
IF(XZV.NE.1..OR.RGZV.NE.1.) DZV = (1.-XZV)**2/(RHOFZB*(1.-RGZV)
1)+DZV
DZB = (1.-XZB)**2/(RHOFZB*(1.-RGZB))+XZB**2/(RHOGZB*RGZB)
IF(ZV.GT.0.0) DABB = (G**2)*(DZV-DZB)
XEZV=1.0
IF(ZV.GE. TL) XEZV=XEOUT
PHLOMN=1.2*((RHOFZB/RHOGZB)-1.)*(XEZV)**.824
DFBB=(G*737.73)**2*FRIC*(PHLOMN*CORFAC/1.824+1.)*(ZV-ZB)/(RHOFZB*
10.06243*2*32.2*3600.**2*D)*47.867
DEVID=((7.04-3.8*XEZV)*(1.172-1.7*PB)+3.4*
1 PB-.344)
IF(IFLAG.GT. 0) DABB=0.
IF(ZV.LT. TL) GO TO 350
DFTOP=G**2*FRIC*(PHLOMN*CORFAC+1.0)*(LTOP+LETOP)/
1 (RHOFZB*D*2.)
IF(JFLAG.GT. 0) DFTOP=DFTOP/DEVID
DETOP=RHOZV*9.81*LTOP
DTTOP=DFTOP+DETOP
350 IF(JFLAG.GT. 0) DFBB=DFBB/DEVID
C WRITE (6,320)
320 FORMAT(1X,'DFBB,FRIC,PHLOMN,CORFAC,ZB,RHOFZB,RHOGZB')
C WRITE(6,121) DFBB,FRIC,PHLOMN,CORFAC,ZB,RHOFZB,RHOGZB
DTBB = DEBB+DABB+DFBB

C
C ITERATIONS OF PRESSURE AT ZV.
C
PVV = (P*1.E6-(DINONB+DTSUB+DTBB+DTBOT))
PVITE = ABS((PVV/1.E6-PV)/PV)
IF(PVITE.GT.0.00005) PV=PVV/1.E6
IF(PVITE.GT.0.00005) GO TO 300
WRITE(6,400) ZV,XZSC,XZB,RGZB,XZV,RGZV,XEOUT,XOUT
400 FORMAT(3X,'ZV= ',F10.4,1X,'M' /
1 3X,'EQUILIBRIUM QUALITY AT ZSC = ',E13.6/
2 3X,'NON EQUILIBRIUM QUALITY AT ZB = ',E13.6/
3 3X,'MARTINELLI-NELSON VOID FRACTION AT ZB = ',F10.4/
4 3X,'NON EQUILIBRIUM QUALITY AT ZV = ',E13.6/
5 3X,'MARTINELLI-NELSON VOID FRACTION AT ZV = ', E13.6/
6 3X,'QUALITY AT CHANNEL OUTLET , EQ = ',F10.4,' NON EQ = ',F10.4)
IF(ZV.GE.TL) GO TO 625

C
C DETERMINATION OF VAPOR DENSITY AT EXIT.
C
HTL = Q(I)*1.E3*PI*DROD*TL/MDOT+HIN
TG = TSAT+2.
IF(PV*1.E6.GT.2.E6) GO TO 500
ES = C6+C7*(1./(C8+PV*1.E6))
GS = C9+(C11*PV*1.E6+C10)*PV*1.E6
GO TO 510

```

```

500 ES = C12+(C14*PV*1.E6+C13)*PV*1.E6
    GS = C15+(C17*PV*1.E6+C16)*PV*1.E6
510 CPS = C4*(1.0-A15*TSAT)**C5
    BETA = TSAT**2*(1.0-1.0/(A11*CPS-1.0)**2)
520 EG = ES+A12*((TG-TSAT)+(TG**2-BETA)**.5-TSAT/(A11*CPS-1.0))
    DENG = PV*1.E6/((GS-1.0)*ES+C26*(EG-ES))
    HG = EG+PV*1.E6/DENG
    HABS = ABS((HG/1.E3-HTL)/HTL)
    IF(TG.GT.700.) GO TO 530
    IF(HABS.GT.0.005) TG = TG+1.
    IF(HABS.GT.0.005) GO TO 520
C
C SINGLE PHASE VAPOR PRESSURE DROPS. THESE PRESSURE DROPS MAY NOT BE
C COMPATIBLE WITH THOSE CALCULATED EARLIER AND ARE NOT TABULATED.
C
530 TBA = TG-0.5*(TG-TSAT)
    IF(TBA.GT.640.) TBA = 640.
    IF(TBA.GT.640.) WRITE(6,570)
570 FORMAT(3X,'THE AV. VAPOR TEMP. HAS EXCEEDED THE RANGE OF VALIDITY
1OF THE VAPOR VISCOSITY CORRELATION. SO AS TO AVOID A SUBSEQUENT NE
2GATIVE ARGUMENT,TBA IS TAKEN TO BE 640. K')
    UBG = UG(TBA)
    RE = G*D/UBG
C    FRIC = .316/RE**.25
    DEVAP = 0.5*(RHOGZB+DENG)*9.81*(TL-ZV)
    DAVAP = G**2*(1./DENG-1./RHOGZB)
C    DFVAP = FRIC*G**2*(TL-ZV)/(2.*D*0.5*(RHOGZB+DENG))
    PHOLMN=1.2*(RHOFZB/RHOGZB-1.)
    DFVAP=FRIC*G**2.*(TL-ZV)*(PHOLMN*CORFAC+1.)/(RHOFZB
1 *D*2.)
    DFTOP=FRIC*G**2.*(LTOP+LETOP)*(PHOLMN*CORFAC+1.)/(RHOFZB*D*2.)
    IF(IFLAG .GT. 0) DAVAP=0.0
C    DFVAP = DFVAP+FRIC*G**2*(LTOP+LETOP)/(2.*D*DENG)
    DETOP=DENG*9.81*LTOP
    IF(JFLAG .LE. 0) GO TO 580
    DFVAP=DFVAP/DEVID
    DFTOP=DFTOP/DEVID
580 DTTOP=DETOP+DFTOP
    DTVAP = DEVAP+DAVAP+DFVAP
    WRITE(6,600) TG,HTL,DENG,HG,RE,DEVAP,DAVAP,DFVAP,DTVAP
600 FORMAT(3X,'VAPOR TEMPERATURE AT EXIT = ',F10.3,1X,'K'/3X,'ENTHALPY
1 AT EXIT(HEAT BALANCE)= ',F10.1,1X,'KJ/KG'/3X,'VAPOR DENSITY AT EX
2IT = ',F10.3,1X,'KG/M**3'/3X,'ENTHALPY AT EXIT(CORRELATED) = ',F10
3.1,1X,'J/KG'/3X,'VAPOR REYNOLDS NUMBER = ',F10.1/3X,'ELEVATION VAP
4OR PR. DROP = ',F10.3,1X,'PA'/3X,'ACCELERATION VAPOR PR. DROP = ',
5F10.3,1X,'PA'/3X,'FRICTION VAPOR PR. DROP = ',F10.3,1X,'PA'/3X,'TO
6TAL VAPOR PR. DROP = ',F10.2,1X,'PA')
C
C TOTAL PRESSURE DROP.
C
625 DROP = DINONB+DTSUB+DTBB+DTVAP+DITOP+DEBOT+DFBOT
    WRITE(6,650) DROP
650 FORMAT(/3X,'TOTAL PRESSURE DROP = ',F10.0,1X,'PA')
C
C TABULATION OF PRESSURE DROP COMPONENTS
C
    DF = DFNONB+DFSUB+DFBB+DFTOP+DFBOT
    DE = DENONB+DESUB+DEBB+DETOP+DEBOT
    DA = DANONB+DASUB+DABB
    DFCENT = DF/DROP*100.
    DECENT = DE/DROP*100.
    DACENT = DA/DROP*100.
    DTNCEN = DINONB/DROP*100.
    DTSCEN = DTSUB/DROP*100.
    DTBCEN = DTBB/DROP*100.
    WRITE(6,651)
651 FORMAT(/3X,'***** TABULATION OF PRESSURE DROP COMPONENTS IN PAS
1CALS *****')
    WRITE(6,652)
652 FORMAT(3X,'*****')
    WRITE(6,653)
653 FORMAT(13X,'BOILING REGIME SUBTOTAL (COMP./TOT
1AL)%')
    WRITE(6,654)
654 FORMAT(3X,'COMPONENT NON-BOILING SUBCOOLED BULK')
    WRITE(6,655)
655 FORMAT(3X,'*****')
    WRITE(6,656)

```

```

        WRITE(6,656) DFNONB,DFSUB,DFBB,DF,DFCENT
656 FORMAT(3X,'FRICTION',4X,F10.0,1X,3F10.0,8X,F5.2)
        WRITE(6,657) DENONB,DESUB,DEBB,DE,DECENT
657 FORMAT(3X,'ELEVATION',3X,F10.0,1X,3F10.0,8X,F5.2)
        WRITE(6,658) DANONB,DASUB,DABB,DA,DACENT
658 FORMAT(3X,'ACCELERATION',F10.0,1X,3F10.0,8X,F5.2)
        WRITE(6,659)
659 FORMAT(3X,'*****')
1*****')
        WRITE(6,660)
660 FORMAT(50X,'TOTAL')
        WRITE(6,661) DTINONB,DTSUB,DTBB,DROP
661 FORMAT(3X,'SUBTOTAL',4X,F10.0,1X,3F10.0)
        WRITE(6,662)
662 FORMAT(46X,'*****')
        WRITE(6,663) DTINCEN,DTSCEN,DTBCEN
663 FORMAT(3X,'(REGIME/TOTAL)%',1X,F6.2,5X,F6.2,4X,F6.2)
        WRITE(6,675)
675 FORMAT(/3X,'*****')
1*****')
        WRITE(6,676) DETOP,DFTOP,DEBOT,DFBOT
676 FORMAT(3X,'TOP UNHEATED PR. DROP ELEV =' ,F8.2,' FRI=' ,F8.2/
1 3X,'BOTTOM UNHEATED PR. DROP ELEV =' ,F8.2,' FRI=' ,F8.2)
        MDOT=MDOT-DEC
        GO TO 23
700 CONTINUE
1000 FORMAT(7F10.0)
1001 FORMAT(6I5)
        STOP
        END

```

C.....
\$DEBUG

```

        SUBROUTINE INPT(P,DROD,PITCH,TL,TIN,TSAT,HIN,MASS,DEC,MINM,
        1LBOT,LTOP,LEBOT,LETOP,IFLAG,JFLAG,KFLAG,NQ,Q,NSET)
        CHARACTER*23 HEAD(21)
        DIMENSION X(20),IX(10),Q(30)
        REAL MASS,MDOT,MINM,LBOT,LTOP,LEBOT,LETOP
        DATA HEAD/'PEDROP INPUT ', '# INPUT SETS -I',
        1 'PRESSURE(MPA) -R', 'ROD DIAMETER(M) -R',
        2 'C-TO-C DIST. (M)-R', 'CH.AXIAL LEN (M)-R',
        3 'INLET TEMP. (K)-R', 'SAT. TEMP. (K)-R',
        4 'INLET ENTHAL.(KJ/KG)-R', 'HIGH MFR(KG/SEC) -R',
        5 'MFR DECREM. (KG/SEC)-R', 'LOW MFR (KG/SEC)-R',
        6 'BOT.UNHTD LEN(M)-R', 'TOP UNHTD LEN(M)-R',
        A 'BOT.LEN. LOSS(M)-R', 'TOP LEN. LOSS(M)-R',
        7 '# HEAT FLUXES-I', 'IFLAG -I',
        8 'JFLAG -I', 'KFLAG -I',
        9 'HEAT FLUXES (MW/M2)-R'/
        WRITE(*,324)HEAD(1),HEAD(1),HEAD(1)
324 FORMAT(1X,A15,A15,A15)
        II=2
325 FORMAT(I4,5X,A23,'---->'\)
        WRITE(*,325) II,HEAD(2)
        READ(*,300) NSET
        DO 100 I=1,14
        II=I+2
        WRITE(*,325) II,HEAD(II)
        READ(*,200)X(I)
100 CONTINUE
200 FORMAT(F10.0)
        DO 110 I=1,4
        II=I+16
        WRITE(*,325) II,HEAD(II)
        READ(*,300) IX(I)
110 CONTINUE
300 FORMAT(BN,I10)
        NQ=IX(1)
        II=21
        WRITE(*,325) II,HEAD(II)
C        DO 120 I=1,NQ
        READ(*,*)(Q(I),I=1,NQ)
C 120 CONTINUE
10 WRITE(*,400)
400 FORMAT(' YOUR INPUT LOOKS LIKE THIS')
        DO 500 I=1,14
        II=I+2
        WRITE(*,325) II,HEAD(II)
        WRITE(*,*)X(I)

```

```

500 CONTINUE
    DO 510 I=1,4
        II=I+16
        WRITE(*,325) II,HEAD(II)
        WRITE(*,*)IX(I)
510 CONTINUE
    II=21
        WRITE(*,325)II,HEAD(21)
        WRITE(*,*)(Q(I),I=1,NQ)
55 WRITE(*,450)
450 FORMAT(' ENTER A SINGLE INTEGER'/' TO CHANGE AN ENTRY--1'/'
1' TO STOP EXECUTION --2'/' TO CONTINUE      --3')
    READ(*,300)ICK
    GO TO (700,800,600) ,ICK
        GO TO 55
800 STOP
600 P=X(1)
    DROD=X(2)
    PITCH=X(3)
    TL=X(4)
    TIN=X(5)
    TSAT=X(6)
    HIN=X(7)
    MASS=X(8)
    DEC=X(9)
    MINM=X(10)
    LBOT=X(11)
    LTOP=X(12)
    LEBOT=X(13)
    LETOP=X(14)
    IFLAG=IX(2)
    JFLAG=IX(3)
    KFLAG=IX(4)
    GO TO 50
700 WRITE(*,530)
530 FORMAT(' ENTER THE INDEX NUMBER OF ITEM TO BE CHANGED '\)
    READ(*,300) II
    WRITE(*,325) II,HEAD(II)
    IF(II.LT.17) THEN
        READ(*,200)X(II-2)
    ELSEIF(II.EQ.21) THEN
        READ(*,*)(Q(I),I=1,NQ)
    ELSE
        READ(*,300)IX(II-16)
        NQ=IX(1)
        ENDIF
    GO TO 10
50 CONTINUE
C RETURN
END
C.....
SUBROUTINE STATE(P,TV,TL,ROV,ROL,EV,EL,TSAT,HVS,HLS,DTSDP,
1 DELDP,DEVDP,DELDT,DEVDT,DRLDP,DRVDP,DRLDT,DRVDT,IOP,IERR)
C
C
C SUBROUTINE STATE CALCULATES THE STATE DYNAMIC PROPERTIES OF WATER
C
C SI UNITS ARE USED
C
C INPUT VARIABLES
C 1. P PRESSURE
C 2. TL TEMPERATURE OF THE LIQUID
C 3. TV TEMPERATURE OF THE VAPOR
C 4. IOP OPTION SELECTOR - NOT IN PRESENT VERSION
C
C OUTPUT VARIABLES
C 1. EV INTERNAL ENERGY OF THE VAPOR
C 2. EL INTERNAL ENERGY OF THE LIQUID
C 3. TSAT SATURATION TEMPERATURE
C 4. HVS VAPOR SATURATION ENTHALPY
C 5. HLS LIQUID SATURATION ENTHALPY
C 6. ROL DENSITY OF THE LIQUID
C 7. ROV DENSITY OF THE VAPOR
C 8. DTSDP DERIVATIVE OF TSAT WRT PRESSURE
C 9. DELDP DERIVATIVE OF TL WRT PRESSURE
C 10. DEVDP DERIVATIVE OF TV WRT PRESSURE
C 11. DELDT DERIVATIVE OF EL WRT TL
C 12. DEVDT DERIVATIVE OF EV WRT TV
C 13. DRLDP DERIVATIVE OF ROL WRT PRESSURE

```



```

C      12. DRVDP  DERIVATIVE OF ROV WRT PRESSURE -1000
C      13. DRLDT  DERIVATIVE OF ROL WRT TL -1010
C      14. DRVDT  DERIVATIVE OF ROV WRT TV -1020
C      15. IERR   ERROR FLAG (INPUT VARIABLE OUT OF RANGE) -1030
C -1040
C      CONSTANTS USED IN FITS -1050
C -1060
C      FOR TSAT, CPS -1070
C      DATA TSC1,TSC2, TSEXP /9.0395, 255.2, 0.223/ -1080
C      DATA CPS1,CPS2, CPSEXP /9.5875E2, .00132334, -0.8566/ -1090
C      CPS2 = -CPSEXP * TCRINV -1100
C      FOR ES, GAMS IF P < 20 BARS -1110
C      DATA G11,G12,G13 /2.6194106E6, -4.995E10, 3.403E5/ -1120
C      DATA G14,G15,G16 /1.0665544, 1.02E-8, -2.548E-15/ -1130
C      G11,G14 ARE ADJUSTED SO THAT ES RESP. GAMS JUMPS LESS THAN -1140
C      1 PART IN 1.E-8 ACROSS P = 20 BARS. -1150
C      DATA G17 /-5.096E-15/ -1160
C      G17 = 2.* G16 -1170
C      FOR ES, GAMS IF P > 20 BARS -1180
C      DATA G21,G22,G23 /2.5896E6, 6.350E-3, -1.0582E-9/ -1190
C      DATA G24,G25,G26 /1.0764, 3.625E-10, -9.063E-17/ -1200
C      DATA G27,G28 /-2.1164E-9, -18.126E-17/ -1210
C      G27 = 2.* G23, G28 = 2.* G26 -1220
C -1230
C      FOR HLS AND HVS -1240
C      DATA HL0,HL1,HL2,HL3,HL4,HL5/5.7474718E5,2.0920624E-1, -1250
C      1 -2.8051070E-8,2.3809828E-15,-1.0042660E-22,1.6586960E-30/ -1260
C      DATA HV0,HV1,HV2,HV3,HV4/2.7396234E6,3.758844E-2, -1270
C      1 -7.1639909E-9,4.2002319E-16,-9.8507521E-24 / -1280
C -1290
C      DATA P20B /2.0E6/ -1300
C      DATA TCRIT /647.3/ -1310
C      DATA TCRINV /.00154488/ -1320
C      DATA CC,CCI,CCM /1.3, .76923, 0.3/ -1330
C -1340
C      FOR ROL IF T < 576.5 DEG K -1350
C -1360
C      DATA RL0,RL1,RL2,RL3 /1735.3320,-4.6406842,1.0431090E-2, -1370
C      1 -9.4367085E-6/ -1380
C      DATA RL22,RL33 /2.086218E-2,-2.8310126E-5 / -1390
C      RL22 = 2.*RL2 RL33 = 3.*RL3 -1400
C -1410
C      FOR ROL IF T > 576.5 DEG K -1420
C -1430
C -1440
C      DATA RH0,RH1,RH2,RH3,RH4 /-1.1755984E6,8.1437361E3,-2.1136559E1, -1450
C      1 2.4381598E-2,-1.0549747E-5 / -1460
C      DATA RH22,RH33,RH44 /-4.2273118E1,7.3144794E-2,-4.2198988E-5/ -1470
C      RH22 = 2.*RH2 RH33 = 3.*RH3 RH44 = 4.*RH4 -1480
C -1490
C      DATA RP0,RP1,RP2 /-14.643890,1.1283357E-3,1.2670366E-2/ -1500
C -1510
C      DATA SP0,SP1,SP2,SP3 / -42.0218, .2116, -4.4587E-4,3.251E-7/ -1520
C      DATA SP22,SP33 /-8.9174E-4,9.753E-7/ -1530
C -1540
C      FOR EL IF TL < 576.5 DEG K -1550
C      DATA SL0,SL1,SL2,SL3,SL4 /-460.26818E3,-2.8634045E3,27.450693, -1560
C      1 -4.8108323E-2,3.2059316E-5/ -1570
C      DATA SL22,SL33,SL44 /54.901386,-.14432497,1.2823726E-4/ -1580
C      SL22 = 2.* SL2, SL33 = 3.* SL3 -1590
C      FOR EL IF TL > 576.5 DEG K -1600
C      DATA SH0,SH1,SH2,SH3,SH4 /1.2426455E9,-8.6082251E6,2.2364564E4, -1610
C      1 -2.5815959E1,1.1178766E-2/ -1620
C      DATA SH22,SH33,SH44 /4.4729128E4,-77.447877,4.4715064E-2/ -1630
C      SH22 = 2.* SH2, SH33 = 3.* SH3 -1640
C -1650
C      FOR VAPOR -1660
C      DATA A11,A12,A13 /1.2959E-3, 593.59, 1.6847E-3/ -1670
C -1680
C      DATA HALF,ZERO,ONE,TWO /0.5, 0., 1., 2./ -1690
C -1700
C ----- -1710
C -1720
C      CHECK THAT P, TL, TV, ARE WITHIN RANGE OF FITS -1730
C -1740
C      TLSAVE = TL -1750
C      IF(TL.GT.647.) TL = 647. -1760
C      IF (P.GE.1.0E+3.AND.P.LE.190.0E+5) GO TO 5 -1770
C      IERR = 1 -1780

```

RETURN	-1790
5 IF (TL.GE.280.0.AND.TL.LE.647.0) GO TO 10	-1800
IERR = 2	-1810
RETURN	-1820
10 IF(TV.GE.280.0) GO TO 20	-1830
IERR = 3	-1840
RETURN	-1850
20 IERR = 0	-1860
C	-1870
C CALCULATE SATURATION PROPERTIES	-1880
C	-1890
C 1. TSAT SATURATION TEMPERATURE	-1900
C 2. DTSDP DERIVATIVE OF TSAT WRT PRESSURE	-1910
C 3. ES SATURATION INTERNAL ENERGY	-1920
C 4. DPES DERIVATIVE OF ES WRT PRESSURE	-1930
C 5. GAMS GAMMA SUB S	-1940
C 6. DPGAMS DERIVATIVE OF GAMS WRT PRESSURE	-1950
C 7. CPS C SUB PS	-1960
C 8. DPCPS DERIVATIVE OF CPS WRT PRESSURE	-1970
C 9. GAMSM GAMS-ONE	-1980
C 10. HVS VAPOR SATURATION ENTHALPY	-1990
C 11. HLS LIQUID SATURATION ENTHALPY	-2000
C	-2010
TSAT = TSC1* P**TSEXP	-2020
HVS = HV0 + P*(HV1 + P*(HV2 + P*(HV3 + P*HV4)))	-2030
HLS = HL0 + P*(HL1 + P*(HL2 + P*(HL3 + P*(HL4 + P*HL5))))	-2040
PINV = ONE/ P	-2050
DTSDP = TSAT*TSEXP*PINV	-2060
TSAT = TSAT + TSC2	-2070
C	-2080
T1 = ONE - TSAT*TCRINV	-2090
CPS = CPS1* T1**CPSEXP	-2100
DPCPS = CPS2*CPS/T1 *DTSDP	-2110
C	-2120
IF (P.GT.P20B) GO TO 150	-2130
T2 = ONE/ (G13+P)	-2140
T1 = T2*G12	-2150
ES = G11 + T1	-2160
DPES = -T1*T2	-2170
GAMS = G14 + P*(G15 + P*G16)	-2180
DPGAMS = G15+G17*P	-2190
GO TO 200	-2200
150 CONTINUE	-2210
ES = G21+(G23*P+G22)*P	-2220
DPES = G22+G27*P	-2230
GAMS = G24+(G26*P+G25)*P	-2240
DPGAMS = G25 + G28*P	-2250
200 GAMSM = GAMS - ONE	-2260
C	-2270
C	-2280
C CALCULATE LIQUID PROPERTIES	-2290
C	-2300
C	-2310
C 1. INTERNAL ENERGY AND ITS DERIVATIVES	-2320
C	-2330
DP=P - 150.E5	-2340
DELDP = -EXP(SP0+TL*(SP1+TL*(SP2+TL*SP3)))	-2350
DEL = DELDP * DP	-2360
IF (TL.GE.576.5) GO TO 210	-2370
EL = SL0 + TL*(SL1 + TL*(SL2 + TL*(SL3+TL*SL4))) + DEL	-2380
DELDLT = SL1 + TL*(SL22 + TL*(SL33+TL*SL44))	-2390
1 + DEL * (SP1 + TL*(SP22 + TL*SP33))	-2400
GO TO 220	-2410
210 CONTINUE	-2420
EL =(SH0 + TL*(SH1 + TL*(SH2 + TL*(SH3+ TL*SH4)))) + DEL	-2430
DELDLT = (SH1 + TL*(SH22 + TL*(SH33 + TL*SH44)))	-2440
1 + DEL * (SP1 + TL*(SP22 +TL*SP33))	-2450
220 CONTINUE	-2460
C	-2470
C 2. DENSITY AND ITS DERIVATIVES	-2480
C	-2490
DRLDP = EXP(RP0 + RP1*EXP(RP2 * TL))	-2500
DRL = DRLDP * DP	-2510
IF (TL.GE.576.5) GO TO 230	-2520
ROL = RL0 + TL*(RL1 + TL*(RL2+ TL*RL3)) + DRL	-2530
DRLDT = RL1 + TL*(RL22 + TL*RL33) + DRL*RP1*RP2*EXP(RP2*TL)	-2540
GO TO 240	-2550
230 CONTINUE	-2560
ROL = RH0 + TL*(RH1 + TL*(RH2 + TL*(RH3 + TL*RH4))) + DRL	-2570

```

      DRLDT = RH1 + TL*(RH22 + TL*(RH33 + TL*RH44)) + -2580
1      DRL*RP1*RP2*EXP(RP2*TL) -2590
240 CONTINUE -2600
      TL = TLSAVE -2610
C -2620
C CALCULATE VAPOR PROPERTIES -2630
C -2640
      DT = TV-TSAT -2650
      IF (DT.LE.ZERO) GO TO 250 -2660
C -2670
C SUPERHEATED VAPOR -2680
C -2690
C      1. BETA A WORKING PARAMETER -2700
C      2. CAPK A WORKING PARAMETER -2710
C      3. DBETAP DERIVATIVE OF BETA WRT PRESSURE -2720
C      4. DCAPKP DERIVATIVE OF CAPK WRT PRESSURE -2730
C      5. DEVDT -2740
C      6. DEVDP -2750
C      7. ROV -2760
C      8. DRVDE -2770
C      9. DRVDP -2780
C -2790
      T1 = ONE/(A11*CPS-ONE) -2800
      T1SQ = T1*T1 -2810
      BETA = TSAT*TSAT*(ONE - T1SQ) -2820
      T2 = TSAT*T1 -2830
      DE = A12*(DT+SQRT(TV*TV-BETA)-T2) -2840
      EV = ES + DE -2850
      CAPK = A13*DE+TSAT+T2 -2860
      DBETAP = TWO*(BETA*DTSDP+T2*T2*T2*A11*DPCPS)/TSAT -2870
      DCAPKP = -A13*DPES + (ONE + T1)*DTSDP -2880
1      -TSAT*A11*T1SQ*DPCPS -2890
      T3 = ONE-BETA/(CAPK*CAPK) -2900
      DEVDT = ONE/(HALF*T3*A13) -2910
      DEVDP = -HALF*(T3*DCAPKP+DBETAP/CAPK)*DEVDT -2920
      T4 = ONE/(GAMSM*ES+CCM*DE) -2930
      ROV = P*T4 -2940
      DRVDE = -ROV*CCM*T4 -2950
      DRVDT = DRVDE*DEVDT -2960
      DRVDP = ROV*(PINV-(ES*DPGAMS+(GAMSM-CCM)*DPES)*T4) -2970
1      + DRVDE*DEVDP -2980
      GO TO 300 -2990
250 CONTINUE -3000
C -3010
C SUBCOOLED VAPOR -3020
C -3030
      DEVDT = CPS * CCI -3040
      DE = DT * DEVDT -3050
      EV = ES + DE -3060
      T1 = ONE/ CPS -3070
      DEVDP = -(DTSDP -CC*T1*(DPES +DE*DPCPS*T1) )*DEVDT -3080
      T1 = ONE/ GAMSM -3090
      T2 = ONE/ EV -3100
      ROV = P *T1*T2 -3110
      DRVDE = -ROV *T2 -3120
      DRVDT = DRVDE * DEVDT -3130
      DRVDP = ROV *(PINV - DPGAMS*T1) + DRVDE*DEVDP -3140
C -3150
300 CONTINUE -3160
      RETURN -3170
      END -3180
C .....
C *****
      FUNCTION RHOF(TBA)
C *****
      RHOF=-4276.+53.24*TBA-.1953*TBA**2+3.097E-4*TBA**3-1.824E-7*TBA**4
      RETURN
      END
C *****
      FUNCTION RHOG(TBA,PB)
C *****
C UNIT = KG/M**3
      RHOG = .576+PB*1.E6*(2.483E-5-1.41E-12*PB*1.E6)+(PB*1.E6/TBA)*(-2.
1616E-2+1.016E-9*PB*1.E6+7.589/TBA)
      RETURN
      END
C *****
      FUNCTION CP(TBA)
C *****

```

```

C  UNIT = J/KG K
    CP = 4028.+128.8/(1.-TBA/650.)+4.674/((1.-TBA/650.)**2)
    RETURN
    END
C  *****
    FUNCTION TKCOOL(TBA,P)
C  *****
C  UNIT = W/M K
    TKCOOL = .686+7.3E-10*P*1.E6-5.87E-6*(TBA-415.)**2
    RETURN
    END
C  *****
    FUNCTION UF(TBA)
C  *****
C  UNIT = KG/M SEC
    UF = 25.3/(-8.58E4+91.*TBA+TBA**2)
    RETURN
    END
C  *****
    FUNCTION UG(TBA)
C  *****
    UG = 11.4/(1.37E6-844.*TBA-TBA**2)
    RETURN
    END
C  *****
    FUNCTION ENTHAF(PB)
C  *****
C  UNIT = KJ/KG
    PB = PB*1.4507772E2
    IF(PB.LT.400..OR.PB.GT.2500.) GO TO 7997
    ENTHAF = (3.19328213E2+3.04661960E-1*PB-9.85841140E-5*PB**2+1.7101
11786E-8*PB**3)*2.325837743
    GO TO 7999
7997 WRITE(6,7998)
7998 FORMAT(3X,'THE PRESSURE IS OUT OF THE RANGE OF VALIDITY OF THE SAT
URATED LIQUID ENTHALPY CORRELATION')
7999 PB = PB*6.8928571E-3
    RETURN
    END
C  *****
    FUNCTION ENTHAG(PV)
C  *****
    PV = PV*1.4507772E2
    IF(PV.LT.450..OR.PV.GT.2300.) GO TO 8997
    ENTHAG = (1.20742535E3+7.84021105E-3*PV-2.39800695E-5*PV**2+1.0924
16887E-9*PV**3)*2.32587743
    GO TO 8999
8997 WRITE(6,8998)
8998 FORMAT(3X,'THE PRESSURE IS OUT OF THE RANGE OF VALIDITY OF THE SAT
URATED VAPOR ENTHALPY CORRELATION')
8999 PV = PV*6.8928571E-3
    RETURN
    END

```